

Treatment of Zincor Effluent
with Powder Calcium Carbonate
(Sappi Enstra)

by

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Background

- Zincor utilises a typical roast-leach-electrowinning process to produce:
 - super high-grade quality zinc together with several other zinc grades and
 - zinc- aluminium alloys from zinc sulphide concentrates.
- Concentrates are sourced mainly from southern African mines with a portion being imported.

Problems/Shortfalls

- Zincor refinery required management of acidic effluent and impurities such as Mg, Mn, Pb, Si, etc.
- High levels of impurities on the spent electrolyte had a negative effect in terms of:
 - Electrowinning efficiency
 - Plant stability
 - Zinc production and final product
- Lime was used at Zincor to treat final effluent and the disadvantage is high cost.
- Zincor and CSIR embarked on a process to develop and implement technology using CaCO_3

Demonstration Scale



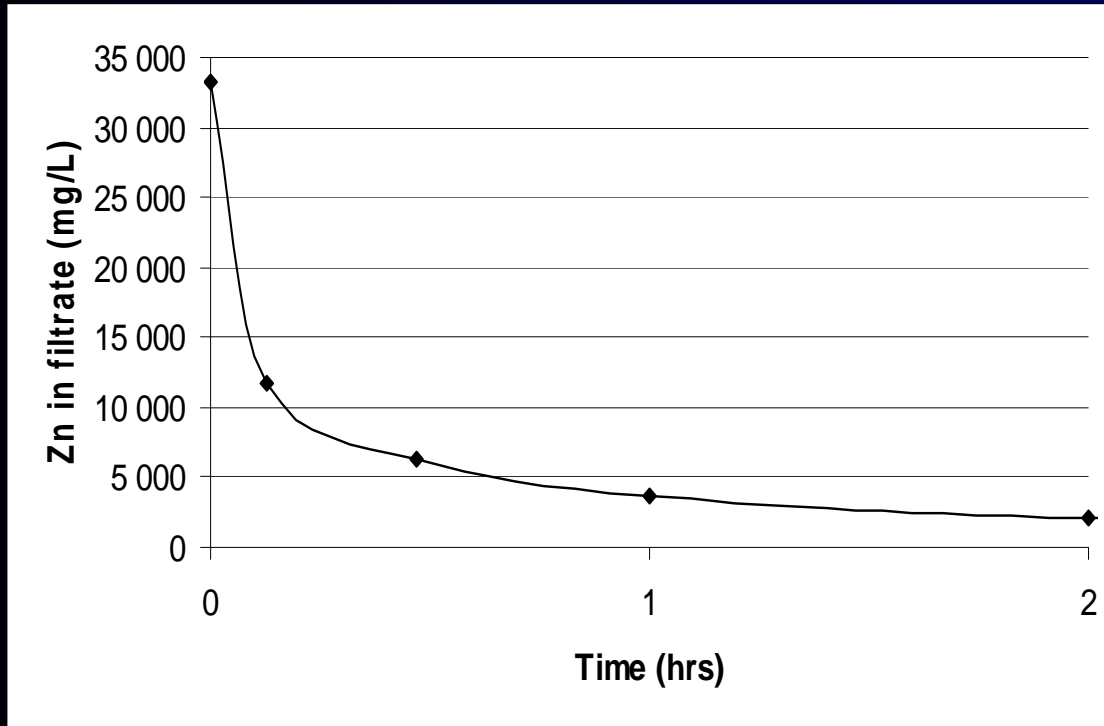
Experimental

- The following conditions were applied for control experiments:
 - Powder CaCO_3 slurry concentration (20%)
 - Excess CaCO_3 concentration (20%)
 - Mixing intensity (2200rpm)
 - Temperature
 - Total active reactor volume

Bed expansion in the vessel

- 30 % bed expansion was experienced in the demonstration unit
- In 60 m³ vessels only 150 to 200 mm bed expansion (< 5%) is expected.
- Smaller volume of air for the specific surface area will be applied

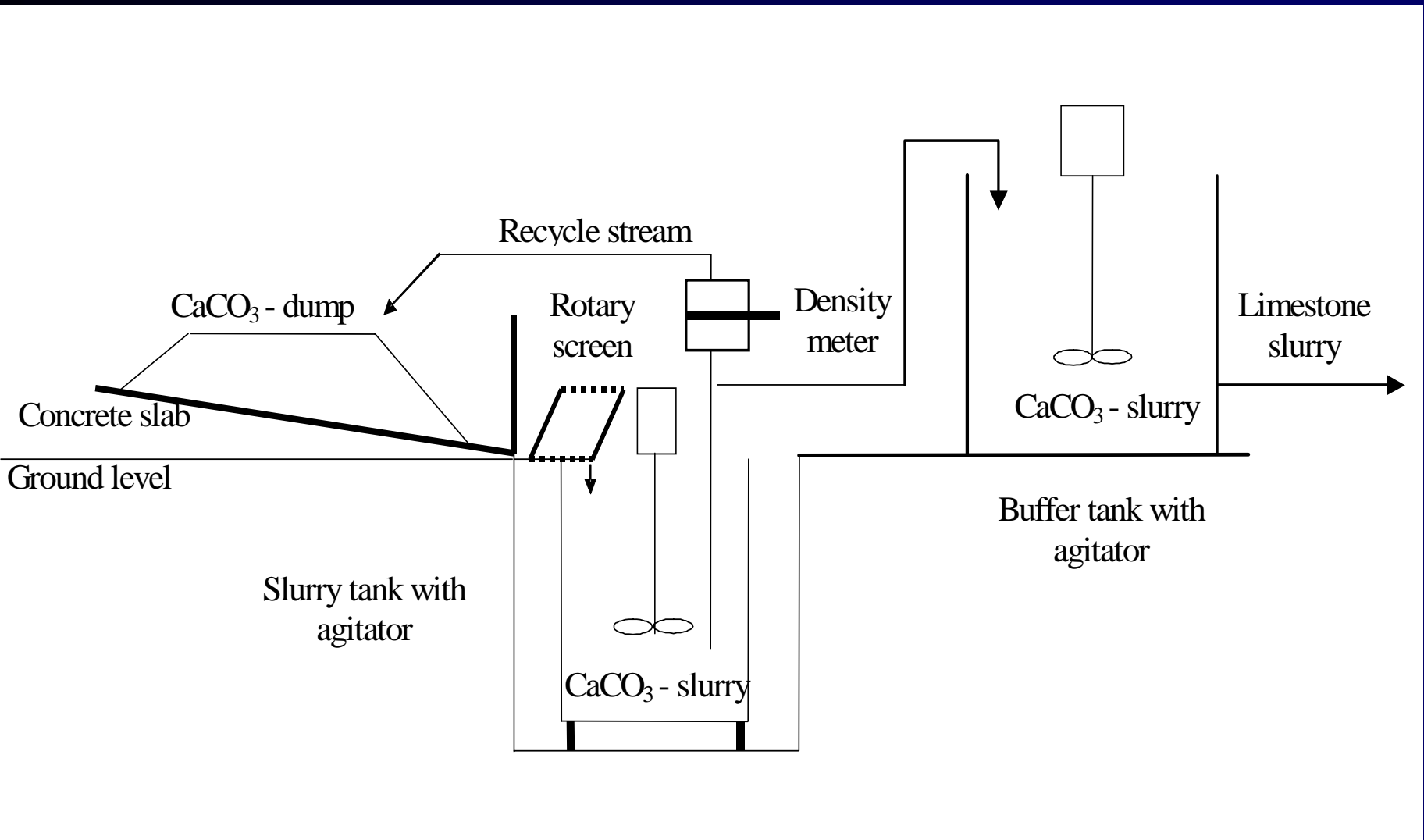
Laboratory test work



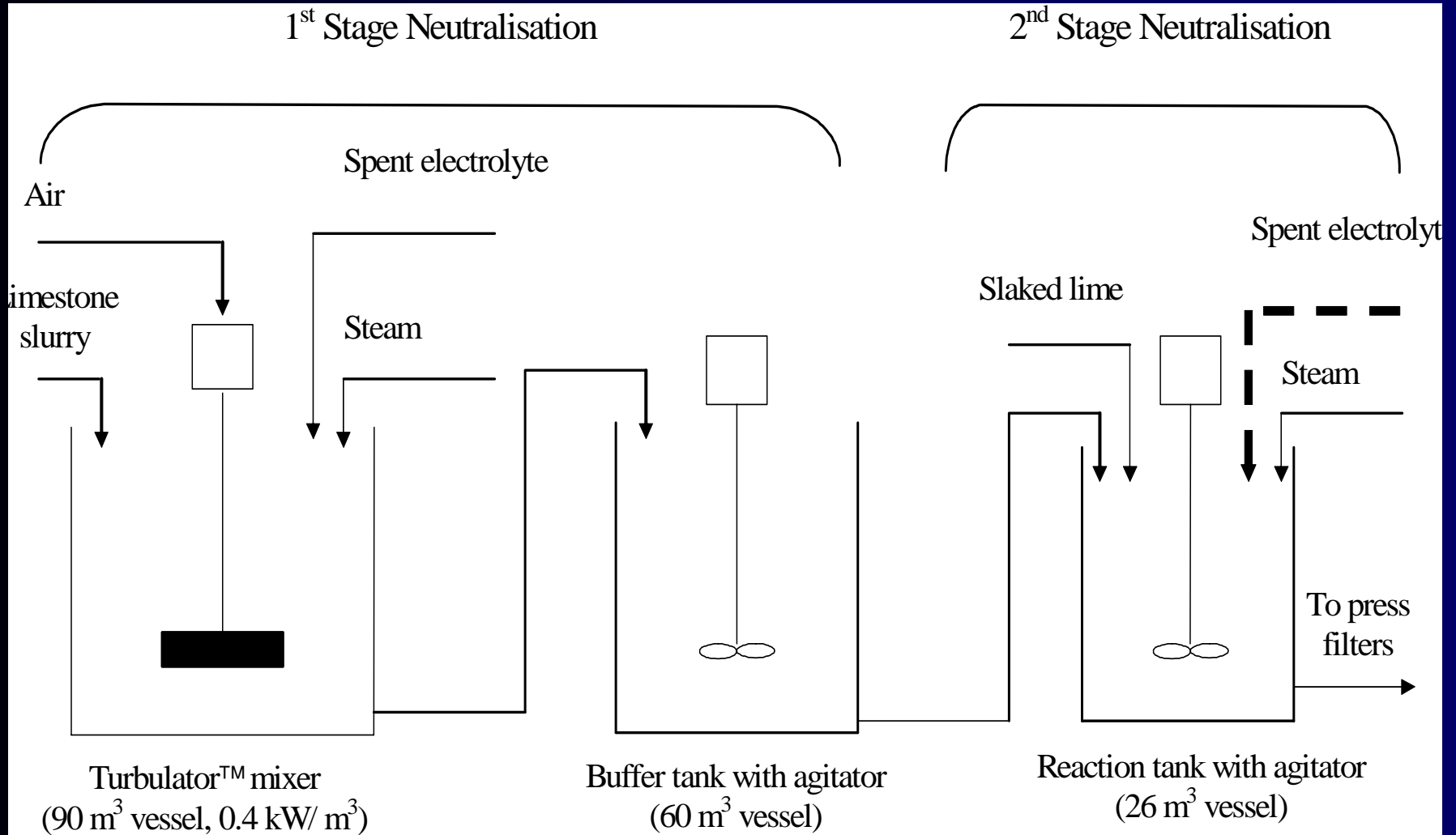
Optimum conditions

- Temp. (70°C)
- Slurry con. (20%)
- CO₂ stripping applied
- Excess CaCO₃ (20%)
- HRT (2hrs and longer)
- High mixing intensity

Schematic diagram of existing plant



Full-scale plant



Plant effluent before and after treatment

| Parameter | Units | Effluent | CaCO ₃ | Lime treated |
|------------|---------------------------|-----------|-------------------|--------------|
| | | (Penstoc) | treated | (Thickener) |
| pH | | 2.6 | 6.6 | 9.3 |
| Sulphate | mg/l as SO ₄ | 11000 | 7300 | 2590 |
| Chloride | mg/l as Cl | 230 | 230 | 230 |
| Fluoride | mg/l as F | 1 | 1 | 1 |
| Alkalinity | mg/l as CaCO ₃ | 0 | 624 | 111 |
| Acidity | mg/l as CaCO ₃ | 6999 | 2988.1 | 0 |
| Sodium | mg/l as Na | 190 | 300 | 312 |
| Calcium | mg/l as Ca | 217 | 400 | 615 |
| Magnesium | mg/l Mg | 300 | 344 | 199 |
| Aluminium | mg/l as Al | 128 | 0.3 | 0.3 |
| Manganese | mg/l as Mn | 325 | 300 | 42 |
| Iron(II) | mg/l as Fe | 55.9 | 0.9 | 0.2 |
| Iron(III) | mg/l as Fe | 91 | 0 | 0 |
| Cobalt | mg/l as Co | 1.7 | 0.2 | 0.2 |
| Nickel | mg/l as Ni | 2.6 | 0.4 | 0.4 |
| Copper | mg/l as Cu | 30 | 0.2 | 0.3 |
| Zinc | mg/l as Zn | 1350 | 1300 | 5.5 |

CSIR/ZINCOR

- The work done by CSIR/ZINCOR involved:
 - Implementation of a handling and dosing system of powder CaCO_3
 - Replacement of lime with powdered CaCO_3 for neutralization of penstock return water
 - Identification of conditions required to neutralize free acid and precipitate zinc from spent electrolyte using powder CaCO_3

Benefits of using CaCO_3

- Full-scale implementation of this technology offered Zincor mine:
 - 75% reduction in lime consumption
 - 55% reduction in the cost of raw material
 - safer and easier handling of neutralizing agent
 - increased neutralization capacity and process stability

Cont.

- Simplified process control
- Minimisation of material wastage
- Elimination of hazardous chemicals used for neutralization
- Utilisation of equipment at existing lime neutralization plants was possible